PRODUCT DATA SHEET

Purolite[®] A200C

Polystyrenic Gel, Type II Strong Base Anion Resin, Chloride form

PRINCIPAL APPLICATIONS

- Demineralization Industrial Water
- Acid Removal

ADVANTAGES

- High operating capacity
- High linear velocity applications
- Reversible sorption of complex ionized and non-ionized organics
- Efficient regeneration
- Good kinetic performance

REGULATORY APPROVALS

- IFANCA Halal Certified
- LPPOM MUI Halal Certified

TYPICAL PACKAGING

- 1 ft³ Sack
- 25 L Sack
- 5 ft³ Drum (Fiber)
- 1 m³ Supersack
- 42 ft³ Supersack
- Bulk Tanker (NA only)

TYPICAL PHYSICAL & CHEMICAL CHARACTERISTICS:

Polymer Structure	Gel polystyrene crosslinked with divinylbenzene
Appearance	Spherical Beads
Functional Group	Type II Quaternary Ammonium
Ionic Form	CI ⁻ form
Total Capacity	1.3 eq/L (28.4 Kgr/ft³) (Cl ⁻ form)
Moisture Retention	45 - 51 % (Cl⁻ form)
Particle Size Range	425 - 1200 μm
< 425 μm (max.)	2 %
Uniformity Coefficient (max.)	1.6
Reversible Swelling, $CI^- \rightarrow OH^-$ (max.)	20 %
Specific Gravity	1.08
Shipping Weight (approx.)	680 - 715 g/L (42.5 - 44.7 lb/ft³)
Temperature Limit	85 °C (185.0 °F) (Cl⁻ form)
Temperature Limit	35 °C (95.0 °F) (OH⁻ form)



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Hydraulic Characteristics

PRESSURE DROP

The pressure drop across a bed of ion exchange resin depends on the particle size distribution, bed depth, and voids volume of the exchange material, as well as on the flow rate and viscosity of the influent solution. Factors affecting any of these parameters such as the presence of particulate matter filtered out by the bed, abnormal compressibility of the resin, or the incomplete classification of the bed—will have an adverse effect, and result in an increased head loss. Depending on the quality of the influent water, the application and the design of the plant, service flow rates may vary from 10 to 40 BV/h.

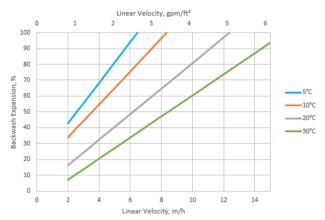
BACKWASH

During up-flow backwash, the resin bed should be expanded in volume between 50 and 70% for at least 10 to 15 minutes. This operation will free particulate matter, clear the bed of bubbles and voids, and reclassify the resin particles ensuring minimum resistance to flow. When first putting into service, approximately 30 minutes of expansion is usually sufficient to properly classify the bed. It is important to note that bed expansion increases with flow rate and decreases with influent fluid temperature. Caution must be taken to avoid loss of resin through the top of the vessel by over expansion of the bed.

Linear Velocity, m/h 80 20 0 40 60 5.0 4.5 100.0 4.0 80.0 3.5 ε psi/ft -15°C 3.0 20°C Drop, 60.0 op, 2.5 =25°C Pressure 2.0 30°C 40.0 1.5 1.0 20.0 0.5 0.0 0.0 35 0 5 10 25 30 40 15 20 Linear Velocity, gpm/ft²

PRESSURE DROP ACROSS RESIN BED

BACKWASH EXPANSION OF RESIN BED





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