PRODUCT DATA SHEET

Purolite[®] A510SMBPlus

Polystyrenic Macroporous, Type II Strong Base Anion Resin, Chloride form, Mixed Bed Grade, Sweetener Grade

PRINCIPAL APPLICATIONS

Deashing - Sugar

Mixed Bed anion component

ADVANTAGES

• Efficient regeneration

SYSTEMS

Mixed Bed

REGULATORY APPROVALS

- Kosher Certified
- IFANCA Halal Certified
- LPPOM MUI Halal Certified

TYPICAL PACKAGING

- 1 ft³ Sack
- 25 L Sack
- 5 ft³ Drum (Fiber)
- 1 m³ Supersack
- 42 ft³ Supersack

TYPICAL PHYSICAL & CHEMICAL CHARACTERISTICS:

Polymer Structure	Macroporous polystyrene crosslinked with divinylbenzene
Appearance	Spherical Beads
Functional Group	Type II Quaternary Ammonium
Ionic Form	CI ⁻ form
Total Capacity	1.15 eq/L (25.1 Kgr/ft³) (Cl ⁻ form)
Moisture Retention	48 - 56 % (Cl⁻ form)
Particle Size Range	425 - 850 μm
< 425 μm (max.)	4 %
Uniformity Coefficient (max.)	1.4
Reversible Swelling, $CI^- \rightarrow OH^-$ (max.)	15 %
Specific Gravity	1.08
Shipping Weight (approx.)	680 - 715 g/L (42.5 - 44.7 lb/ft³)
Temperature Limit	100 °C (212.0 °F) (Cl⁻ form)
Temperature Limit	35 °C (95.0 °F) (OH ⁻ form)



Americas T +1 610 668 9090 F +1 610 668 8139 americas@purolite.com **EMEA** T +44 1443 229334 F +44 1443 227073 europe@purolite.com Asia Pacific T +86 571 876 31382 F +86 571 876 31385 asiapacific@purolite.com FSU T +7 495 363 5056 F +7 495 564 8121 fsu@purolite.com

Hydraulic Characteristics

PRESSURE DROP

The pressure drop across a bed of ion exchange resin depends on the particle size distribution, bed depth, and voids volume of the exchange material, as well as on the flow rate and viscosity of the influent solution. Factors affecting any of these parameters such as the presence of particulate matter filtered out by the bed, abnormal compressibility of the resin, or the incomplete classification of the bed—will have an adverse effect, and result in an increased head loss. Depending on the quality of the influent water, the application and the design of the plant, service flow rates may vary from 10 to 40 BV/h.

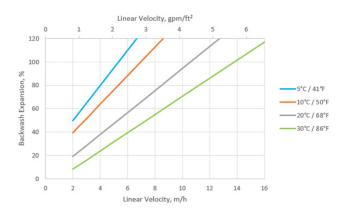
BACKWASH

During up-flow backwash, the resin bed should be expanded in volume between 50 and 70% for at least 10 to 15 minutes. This operation will free particulate matter, clear the bed of bubbles and voids, and reclassify the resin particles ensuring minimum resistance to flow. When first putting into service, approximately 30 minutes of expansion is usually sufficient to properly classify the bed. It is important to note that bed expansion increases with flow rate and decreases with influent fluid temperature. Caution must be taken to avoid loss of resin through the top of the vessel by over expansion of the bed.

Linear Velocity, gpm/ft² 0 10 20 30 40 5 4.5 100 4 kPa/m 80 3.5 -15°C / 59°F ure Drop, 3 -20°C / 68°F 60 2.5 -25°C / 77°F 2 -30°C / 86°F 40 1.5 1 20 0.5 0 0 0 50 60 10 20 30 40 70 80 90 100 Linear Velocity, m/h

PRESSURE DROP ACROSS RESIN BED

BACKWASH EXPANSION OF RESIN BED





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