## Puropack ${ }^{\circledR}$ PPC100H

Polystyrenic Gel, Strong Acid Cation Resin, Hydrogen form, Packed Bed Grade

## PRINCIPAL APPLICATIONS

- Demineralization - Industrial Water


## ADVANTAGES

- High linear velocity applications
- Efficient separation
- Lower pressure drop versus standard resin


## SYSTEMS

- Packed Bed Systems
- Puropack packed bed systems


## REGULATORY APPROVALS

- Kosher Certified


## TYPICAL PACKAGING

- $1 \mathrm{ft}^{3}$ Sack
- 25 L Sack
- $5 \mathrm{ft}^{3}$ Drum (Fiber)
- $1 \mathrm{~m}^{3}$ Supersack
- $42 \mathrm{ft}^{3}$ Supersack

TYPICAL PHYSICAL \& CHEMICAL CHARACTERISTICS:

| Polymer Structure | Gel polystyrene crosslinked with divinylbenzene |
| :--- | :--- |
| Appearance | Spherical Beads |
| Functional Group | Sulfonic Acid |
| lonic Form | $\mathrm{H}^{+}$form |
| Total Capacity | 2 eq/L $\left(43.7 \mathrm{Kgr} / \mathrm{ft}^{3}\right)\left(\mathrm{Na}^{+}\right.$form $)$ |
| Moisture Retention | $51-55 \%\left(\mathrm{H}^{+}\right.$form $)$ |
| Mean Diameter | $650 \pm 50 \mu \mathrm{~m}$ |
| Uniformity Coefficient (max.) | $1.1-1.2$ |
| Reversible Swelling, $\mathrm{Na}^{+} \rightarrow \mathrm{H}^{+}($max. $)$ | $9 \%$ |
| Specific Gravity | $1.2\left(\mathrm{H}^{+}\right.$form $)$ |
| Shipping Weight (approx.) | $745-785 \mathrm{~g} / \mathrm{L}\left(46.6-49.1 \mathrm{lb} / \mathrm{ft}^{3}\right)$ |
| Temperature Limit | $120{ }^{\circ} \mathrm{C}\left(248.0^{\circ} \mathrm{F}\right)$ |

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## Hydraulic Characteristics

## PRESSURE DROP

The pressure drop across a bed of ion exchange resin depends on the particle size distribution, bed depth, and voids volume of the exchange material, as well as on the flow rate and viscosity of the influent solution. Factors affecting any of these parameterssuch as the presence of particulate matter filtered out by the bed, abnormal compressibility of the resin, or the incomplete classification of the bed-will have an adverse effect, and result in an increased head loss. Depending on the quality of the influent water, the application and the design of the plant, service flow rates may vary from 10 to $40 \mathrm{BV} / \mathrm{h}$.

## PRESSURE DROP ACROSS RESIN BED



## BACKWASH

During up-flow backwash, the resin bed should be expanded in volume between 50 and $70 \%$ for at least 10 to 15 minutes. This operation will free particulate matter, clear the bed of bubbles and voids, and reclassify the resin particles ensuring minimum resistance to flow. When first putting into service, approximately 30 minutes of expansion is usually sufficient to properly classify the bed. It is important to note that bed expansion increases with flow rate and decreases with influent fluid temperature. Caution must be taken to avoid loss of resin through the top of the vessel by over expansion of the bed.

BACKWASH EXPANSION OF RESIN BED


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